



Cite this: *Lab Chip*, 2018, 18, 1066

Flow-induced dissolution of femtoliter surface droplet arrays

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The dissolution of liquid nanodroplets is a crucial step in many applied processes, such as separation and dispersion in the food industry, crystal formation of pharmaceutical products, concentrating and analysis in medical diagnosis, and drug delivery in aerosols. In this work, using both experiments and numerical simulations, we *quantitatively* study the dissolution dynamics of femtoliter surface droplets in a highly ordered array under a uniform flow. Our results show that the dissolution of femtoliter droplets strongly depends on their spatial positions relative to the flow direction, drop-to-drop spacing in the array, and the imposed flow rate. In some particular cases, the droplet at the edge of the array can dissolve about 30% faster than the ones located near the centre. The dissolution rate of the droplet increases by 60% as the inter-droplet spacing is increased from 2.5 μm to 20 μm . Moreover, the droplets close to the front of the flow commence to shrink earlier than those droplets in the center of the array. The average dissolution rate is faster for the faster flow. As a result, the dissolution time (T_i) decreases with the Reynolds number (Re) of the flow as $T_i \propto \text{Re}^{-3/4}$. The experimental results are in good agreement with the numerical simulations where the advection–diffusion equation for the concentration field is solved and the concentration gradient on the surface of the drop is computed. The findings suggest potential approaches to manipulate nanodroplet sizes in droplet arrays simply by dissolution controlled by an external flow. The obtained droplets with varying curvatures may serve as templates for generating multifocal microlenses in one array.

Received 11th December 2017,
Accepted 19th February 2018

DOI: 10.1039/c7lc01321c

rsc.li/loc

1 Introduction

Microscopic droplet arrays on surfaces are key to many industrial, technological and analytical processes because of their remarkable properties originating from their microscopic size, large surface-to-volume ratio, long-time stability and defined spatial location. These droplets play a crucial role in the design of novel systems for chemical, catalytic and biological reactions,^{1,2} liquid–liquid extraction for separating or recycling harmful or valuable compounds,^{3,4} or tracing of

analytes in high throughput analysis for environmental, forensic and biomedical monitoring.^{5,6} They are also increasingly applied in drug screening,⁷ optimizing pharmaceutical products, crystallization of proteins,⁸ enzyme detection,^{5,6,9} DNA sequencing,¹⁰ cell culturing¹¹ and assembly of nanomaterials with multifunctionalities.^{12,13}

To be able to control and optimize droplet-based processes, it is crucial to quantitatively understand and control the droplet dynamics in the presence of neighbouring droplets with a high number density. This is essential and urgently needed not only for assembling colloidal particles into functional materials, for accumulating compounds in analyses with single molecule sensitivity,¹⁴ or for producing drugs with the most effective crystalline forms, but also for advanced microfluidic systems as smart drug delivery platforms¹⁵ or as miniaturized chemical reactors with significantly reduced reaction time.¹⁶ These applications of droplets mainly rely on the stability or desirable shrinkage rate of droplets. However, none of the systems studied so far have quantitatively revealed the dynamics of collective droplet dissolution in microfluidic channels where femtoliter surface droplet arrays are exposed to a flowing surrounding phase. A quantitative understanding of collective effects associated with the spatial arrangement of droplets in an external flow is largely missing.

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Recent advances in controlled droplet formation^{17–20} have made it possible to produce femtoliter surface droplet arrays with controllable size, volume and location on a microchannel wall. By the solvent exchange process, we have been able to form highly ordered surface droplet arrays with a designed spatial arrangement on pre-patterned substrates.¹⁹ Surface droplets nucleate and grow exclusively on hydrophobic domains in a constant contact angle mode followed by a constant contact area mode. Such droplet arrays will serve as an ideal model system to quantitatively understand the dynamics of collective droplet dissolution under an external flow.

It is known that shrinking droplets on a substrate exhibit several modes, including a constant contact angle,²¹ a constant contact area,²² a stick-jump,^{23,24} or a mixed mode.²⁵ On a homogeneous smooth surface without chemical patterns, surface nanodroplets with a polydispersed size dissolve in a mixed mode by decreasing both the lateral diameter and the contact angle. Droplets of the same initial size displayed individuality in dissolution rates, due to both pinning and collective effects.^{25,26} In contrast, droplet evaporation on arrays is influenced by convective flow driven by buoyancy.^{21,27} An external flow enhances the dissolution rate of a single entrapped droplet,²⁸ while natural convection plays a role in the dissolution of sub-millimeter drops in a stationary partially miscible liquid.^{29,30} The above situations are all different from the arrangement and dimensions of droplets to be studied in this work.

In the present study, we experimentally and numerically studied the dissolution of droplets in a square packed array. In particular, we looked into how the droplet location and spacing influence their dissolution behavior and how the dissolution of droplets in an array is affected by the surrounding flow. Moreover, we demonstrated that controlled droplet dissolution can be potentially applied to create unconventional microlens arrays with curvature gradients for micro-optical systems.

This paper is organised as follows. In section 2, we describe the experimental technique and the framework for the

numerical simulations. In section 3, we look at the effect of droplet position, spacing and imposed flow rate on the total dissolution time through both experiments and simulations. We conclude the paper with an outlook in section 4.

2 Methods

In Fig. 1(a), we show a schematic of the flow set-up, while in Fig. 1(b) we show the top view along with the notations for the initial droplet lateral diameter (D_0) and the rim-to-rim inter-droplet spacing (S). L is the distance from the first droplet center to the last droplet center in the stream-wise (\hat{e}_x) and span-wise (\hat{e}_y) directions. The position of any drop in the array is normalised using $\tilde{x} = (x - x_0)/L$ and $\tilde{y} = (y - y_0)/L$, where x_0 and y_0 are the center positions of the drop sitting at the corner in the first row, as shown in Fig. 1(b).

2.1 Experiments

Highly ordered droplet arrays are prepared by performing solvent exchange on chemically patterned substrates¹⁹ where ethylene glycol dimethacrylate (EGDMA, 98%, Sigma-Aldrich) is used as liquid oil for forming droplets. In brief, a microfluidic chamber is first filled with solution A containing 10% EGDMA in 50% ethanol–water liquid solution. It is then replaced by water saturated with EGDMA at a flow rate of 200 $\mu\text{L min}^{-1}$. During this solvent exchange, EGDMA droplets nucleate and grow within the hydrophobic domains on the pre-patterned substrates. The number of droplets, D_0 , and S , are determined by the number, size and spacing of circular hydrophobic domains on the substrate.

During dissolution, water (18.2 M Ω cm, Merck Millipore) is injected into the microfluidic chamber with a specific flow rate controlled using a syringe pump. The flow direction is \hat{e}_x (stream-wise), as shown in Fig. 1. Total internal reflection fluorescence (TIRF) microscopy (Nikon N-Storm super resolution confocal microscope) is used to obtain high resolution images of individual dissolving droplets from the bottom view. In this case, 2 μM Nile red ($\geq 98\%$, Sigma-Aldrich) is added into

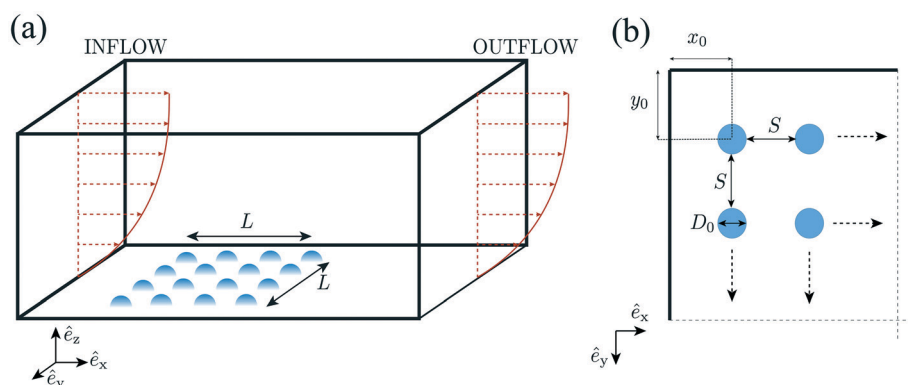


Fig. 1 Schematics of the flow set-up: (a) arrangement of a droplet array of size L in the microfluidic chamber with an imposed flow of fresh water. The chamber height, width and length in the \hat{e}_z , \hat{e}_y and \hat{e}_x directions are 0.63 mm, 15 mm and 63 mm, respectively. (b) Top view of the flow configuration: the initial drop diameter is D_0 and the drops are equidistant from each other with spacing (edge-to-edge) S . The position of the corner drop in the first row is (x_0, y_0) . The dotted arrows indicate a continuing array of drops in the \hat{e}_x and \hat{e}_y directions, up to the array size L .

solution A for making the droplets. Reflection mode optical microscopy (Huvitz HRM-300) with a 50× long focus lens is used to monitor the dissolution process of droplet arrays from the top view. The optical resolution is around 1.6 μm. The shape of the droplets during dissolution can be preserved by photopolymerization. The morphologies of polymerized droplets are then characterized by atomic force microscopy (AFM, Dimension Icon, Bruker). While forming gradient microstructures, glass substrates with pre-patterned surfaces with 40 × 40 domains are used. After an EGDMA droplet array has fully formed, water containing 0.5% 2-hydroxy-2-methyl-propiofenone (97%, Sigma-Aldrich) is injected into the microfluidic chamber. The gradient microstructures obtained after partially dissolving the droplet arrays are photopolymerized by placing the microfluidic chamber under a UV lamp (365 nm, 20 W) for about 15 min. The diffraction patterns of the gradient microstructures under white light illumination are then captured by a colour camera.

2.2 Numerical simulations

We used direct numerical simulations (DNS) to solve the Navier–Stokes equations in a three dimensional Cartesian domain, using a second-order accurate finite-difference scheme with fractional time stepping. The flow solver is coupled with a versatile moving least squares (MLS) based immersed boundary method (IBM) which enforces the interfacial boundary conditions of the immersed drops onto the flow. Additionally, an advection–diffusion type equation is solved for the concentration field. The boundary conditions for the flow set-up are as follows: (i) inflow–outflow in the stream-wise \hat{e}_x direction, (ii) no-slip walls in the wall-normal \hat{e}_z direction, and (iii) periodic in the span-wise \hat{e}_y direction. Hemispherical drops, which are discretised using triangular elements, are placed equidistantly from each other and on the bottom wall, as shown in the schematic in Fig. 1. Through IBM, a free-slip boundary condition is imposed at the interface of the immersed drop and the incoming flow. The concentration field on the surface of the immersed hemispherical drop is kept fixed at saturation throughout the simulation. At any given instant, the concentration gradient on the surface of the immersed drop is computed by interpolating the concentration at the endpoint of a numerical probe normal to every triangular element on the drop surface. The net mass flux from the drop into the flow is computed by summing up the flux from individual triangular elements belonging to an individual drop and the volume of the drop is reduced accordingly. In the simulations, a total of $7 \times 7 = 49$ drops are initialised and allowed to dissolve with an imposed flow rate. It is assumed that the centre of the contact patch of the droplets is fixed, and they dissolve in a constant contact angle (CA) mode, *i.e.* the contact angle of the meniscus in contact with the bottom surface does not change with time.

The droplet liquid density (ρ) is 1051 kg m⁻³, the oil solubility in water (C_s) is 1.086 kg m⁻³ and the diffusion constant is 9.36×10^{-10} m² s⁻¹, in all experiments. The grid resolution for the flow is $720 \times 240 \times 240$ gridpoints in the stream-wise,

span-wise and wall-normal directions, respectively. The immersed drops are initialised with 2592 Lagrangian markers while local adaptive refinement is used as the drops shrink and become smaller. The simulations were run on 48 parallel processors. The Reynolds number of the flow based on the channel height and inflow velocity is set to 0.1. Additional details on the numerical techniques and validation of the code can be found in references.^{31,32}

3 Results and discussion

3.1 Two dissolution modes of an individual droplet

In Fig. 2(a), we show how a single droplet with $D_0 = 10$ μm shrinks within a confined area in a flow of pure water at the rate of 200 μL min⁻¹. Up to 90 s, little change is observed in the lateral size of the droplets, which is attributed to the constant contact radius (CR) dissolution mode. After 120 s, it is apparent that the lateral diameter of the droplet decreases, suggesting a constant contact angle (CA) dissolution mode. The combination of the pinning force on the micropattern boundary and the contact angle of the droplets determines the diameter for the transition of the model.³³

The other noticeable feature is that the three-phase contact line is pinned at one side in CA mode dissolution. This phenomenon suggests that heterogeneities at the boundary of the hydrophobic–hydrophilic region induce strong pinning effects.²⁵ As a consequence, the center of the droplet shifted as well.

The lateral diameter as a function of time is shown in Fig. 2(b). In the CA dissolution mode stage, the dissolution curve shows that the droplet diameter decreases laterally in a steady way, but in a sharp way after it reaches 8 μm. The shape of the droplet during the CA dissolution mode can be experimentally preserved by photopolymerization and further imaged by AFM. Accordingly, we can plot the height of a polymerized droplet as a function of its lateral diameter (Fig. 2(c)). The linear relationship between the lateral diameter and the height confirms the CA dissolution mode. The corresponding contact angle is calculated to be approximately 8.0°, as indicated in (Fig. 2(d)).

The focus in this work is the regime where the droplet shrinks laterally, *i.e.* the CA dissolution mode. We then define the corresponding starting time of the CA dissolution mode as $t = 0$ for the subsequent quantitative analysis.

3.2 Location dependence of droplet dissolution

We will now show the influence of the droplet position in an array on the dissolution behavior in the CA mode. The representative experimental snapshots (Fig. 3(a)) show the overall dissolution process of droplets located in a square packed array. The initial lateral diameter of the drops is $D_0 = 10$ μm while the spacing between the drops is $S = 5$ μm, *i.e.* $S = 0.5D_0$. The dissolution initially occurs on the droplets located at the very corner of the array (*i.e.* $(\tilde{x}, \tilde{y}) = (0, 0)$ and $(\tilde{x}, \tilde{y}) = (0, 1)$), as indicated by black arrows. Strong dissolution effects are first shown at the outer drops and only later for the

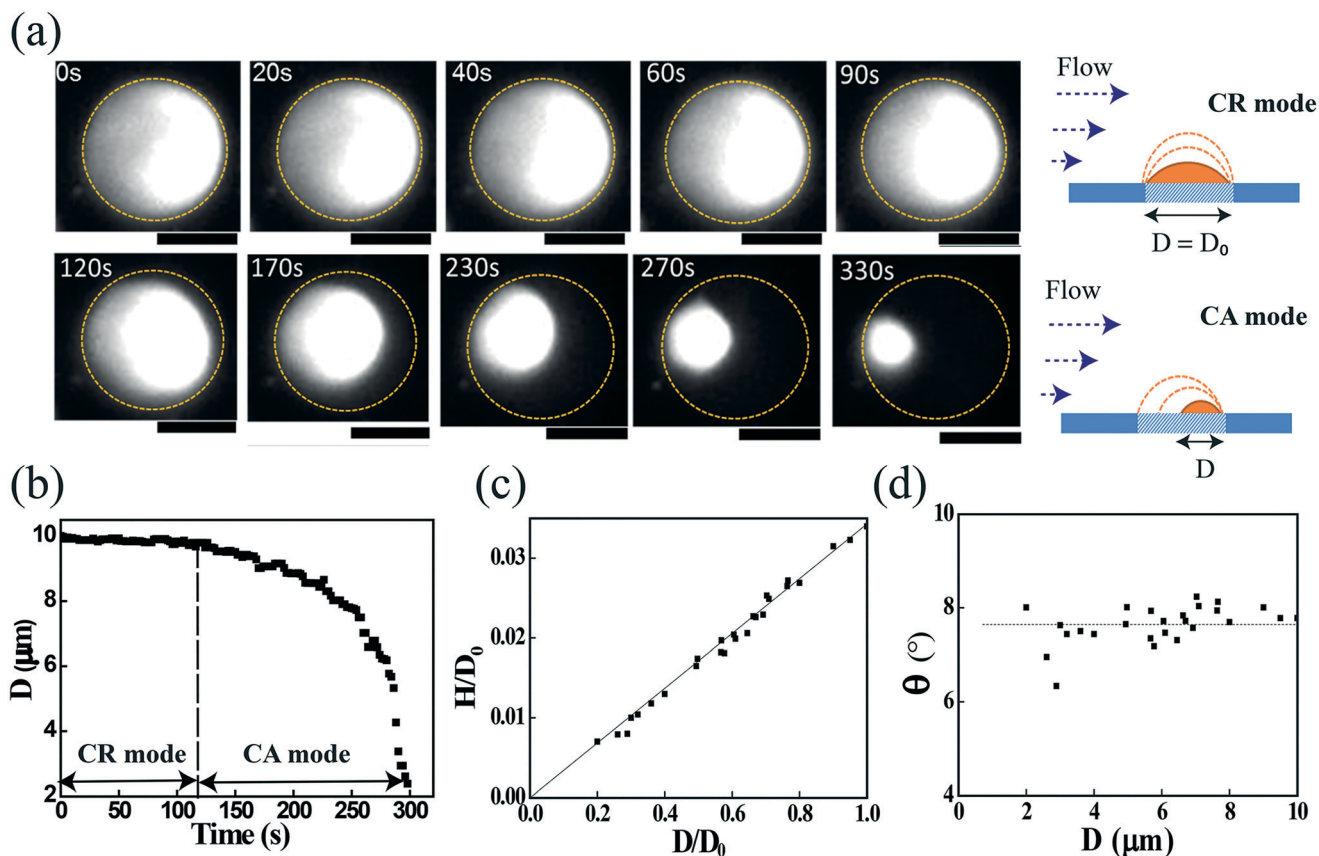


Fig. 2 (a) Time evolution of dissolution of a single droplet monitored by TIRF confocal microscopy. The black scale bars represent a length of 5 μm . The sketches show the corresponding dissolution modes. Top: constant contact area mode (CR mode). Bottom: constant contact angle mode (CA mode). (b) The lateral diameter D shrinks as a function of time during the dissolution. We note that due to the optical resolution limit of the microscope for monitoring the droplets *in situ*, droplets that are smaller than 1.6 μm could not be resolved. (c) The height H of the droplets as a function of the lateral diameter D during the dissolution under the CA mode. The height and lateral diameter are both normalised using D_0 , which is the initial lateral diameter of the drops. (d) The contact angle θ hardly changes with the lateral diameter D under CA mode dissolution.

inner droplets of the array. It is apparent that dissolution is delayed along the stream-wise (\hat{e}_x) direction. The outer droplets in the array act as a shield to the inner droplets. In Fig. 3(b), we show a pseudocolour plot of the concentration field obtained from the numerical simulations. It can be seen that the main features of the flow are very well captured.

To quantify the influence of the spatial position of the drop on its dissolution behaviour, we analyse the dissolution of drops located along specific rows and columns, respectively. In Fig. 4(a), we plot the lateral diameter *versus* time from both experiments and simulations of droplets located in the first column, *i.e.* where the droplets are first hit by the front of the flow.

The experimental measurements displayed in the left panel of Fig. 4(a) clearly show that the droplets at $(\bar{x}, \bar{y}) = (0, 0)$ and $(\bar{x}, \bar{y}) = (0, 1)$ experience a sharp decrease in lateral diameter, while the rest of the drops dissolve more slowly. This feature is also confirmed by the numerical simulations (right panel of Fig. 4(a)), in which the corner drops also dissolve faster than the others. To quantify this, in Fig. 4(b), we plot the total dissolution time (T_i) of individual drops along the

first column ($\bar{x} = 0$), which clearly shows that the dissolution of the corner droplets is about 1.5 times faster than that of the other droplets. We ascribe such a difference to the different local concentration profile, determined by the neighbours of the corresponding droplet, *i.e.* collective effects. In the present case, each corner droplet has two close neighbouring droplets, whereas each inner droplet is surrounded by three close neighbouring droplets. The additional nearby droplets lead to a higher saturation of the surrounding, which results in a reduced dissolution and thus an enhanced dissolution time of the inner droplets. The overall profile displayed in Fig. 4(b) also reflects that the concentration gradient along the span-wise direction of flow changes into a parabolic shape. Compared to the simulated profile in the right panel, the asymmetry in the experimental profile is probably due to some distortion of the flow along the mid $\hat{e}_x - \hat{e}_z$ plane.

As for the droplets along the stream-wise direction, Fig. 4(c) illustrates the diffusive loss of the droplets located in the central row with $\bar{y} = 5$. It is noticeable from both experiments and simulations that in general the dissolution of droplets gradually slows down along the stream-wise (\bar{x})

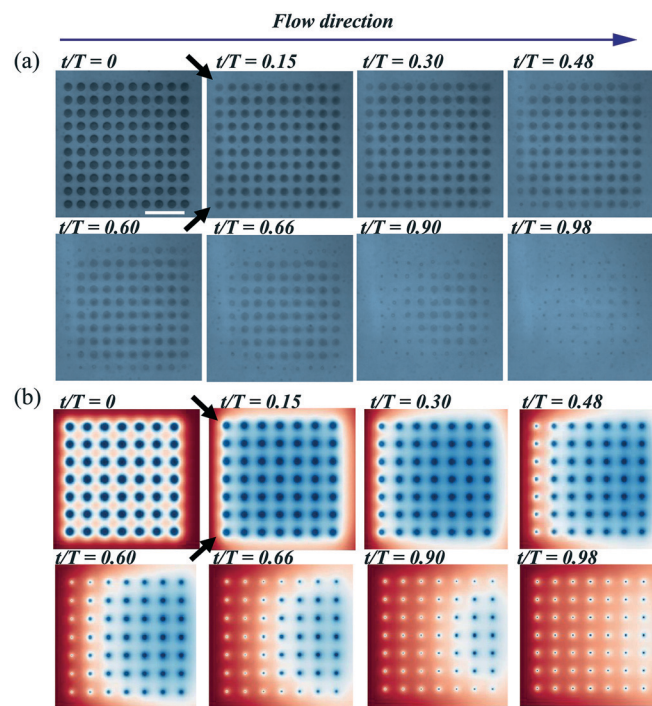


Fig. 3 Time evolution of droplet dissolution: (a) experimental results for a 10×10 droplet array with a spacing of $S = 5 \mu\text{m}$ at a flow rate of $Q = 200 \mu\text{L min}^{-1}$. The length of the scale bar is $45 \mu\text{m}$. (b) The pseudocolour plot of the concentration field from numerical simulations for a 7×7 droplet array for the corresponding flow conditions. Blue and red correspond to oil and water, respectively. The water is injected into the chamber along the \hat{e}_x direction. The black arrows indicate two corner droplets dissolving faster than the other drops. Time t is normalized using T , which is the total time for the droplet array to completely dissolve.

position. The total dissolution time of the corresponding droplets is summarized in Fig. 4(d). The experimental normalized dissolution time has been extended from 0.7 to 1, which is comparable to the normalized simulated time from 0.5 to 1. The quantitative differences observed between the simulations and experiments mainly arise from the assumptions involving pinning, center-shift and dissolution of the drops undertaken in the simulations. The delayed dissolution along the flow direction indicates that the local concentration gradient for the droplet downstream has significantly been reduced by the dissolving upstream neighbours.²⁹

However, there is one exception observed from both the experimental measurements and numerical simulations: the last droplet dissolves much faster than the droplets upstream of it. The reason for this is that the last droplet does not have any drops residing in its wake, which leads to a relatively higher concentration gradient in its wake. This leads to faster dissolution of the last drop or, in other words, a shorter dissolution time. One can expect that when the drops are placed far away from each other, this effect should be reduced and this is indeed observed when we study the effect of inter-droplet spacing on the dissolution behaviour later on. Despite this, the dissolution time of the last droplet is still sig-

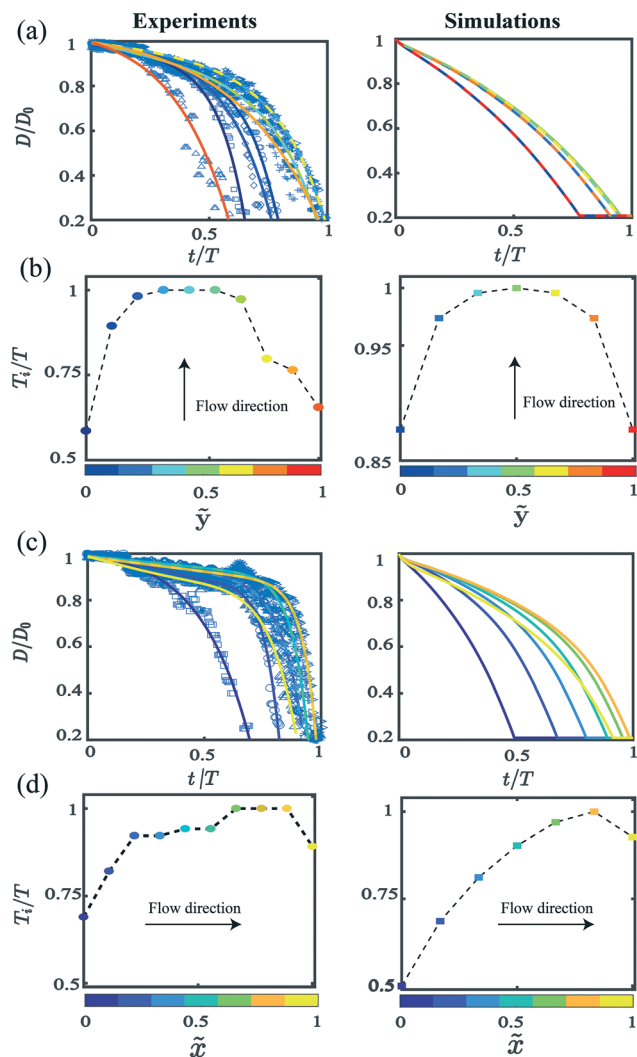


Fig. 4 Time evolution of individual drop diameters in the CA mode from experiments (left column) and numerical simulations (right column) along (a) the span-wise \hat{e}_y and (c) stream-wise \hat{e}_x directions. The total dissolution time (T_i) of droplets along the (b) span-wise and (d) stream-wise directions. In (a) and (b), $\tilde{x} = 0$, i.e. the droplets are located at the first row and face fresh incoming flow, while in (c) and (d), $\tilde{y} = 0.5$, i.e. it is the central column along the streamwise direction. T_i is normalized using $T = \max(T_i)$. The colour bars represent the location of the droplets along the \hat{e}_y direction for (a) and (b) and the \hat{e}_x direction for (c) and (d).

nificantly longer than that of the first droplet, showing the key role of the flow direction.

3.3 Inter-droplet spacing

Next, we examine how the inter-droplet spacing (S) affects the overall dissolution behaviour. In total, four different arrays are prepared with an inter-drop spacing S of $2.5 \mu\text{m}$, $5.0 \mu\text{m}$, $10 \mu\text{m}$, and $20 \mu\text{m}$. Under an imposed flow of water at $200 \mu\text{L min}^{-1}$, droplets with the same relative position (\tilde{x}, \tilde{y}) have different dissolution rates. The representative dissolution behaviour of the droplet situated in the centre of the array with a different S is shown in Fig. 5(a). It can be

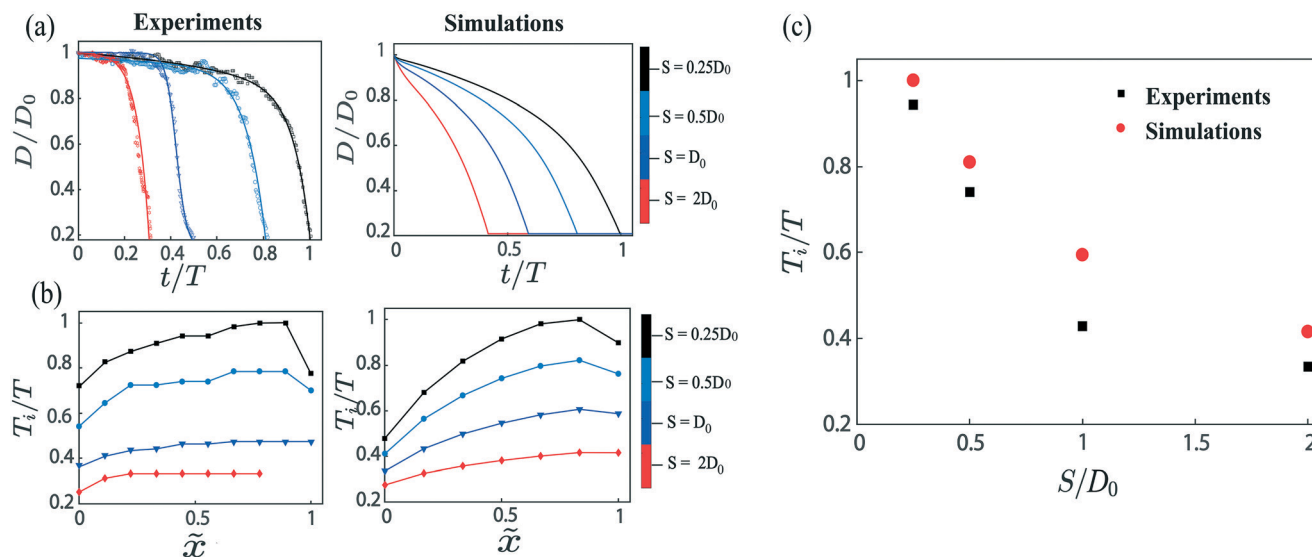


Fig. 5 Droplet dissolution depends on the inter-droplet spacing S : (a) time evolution of the central drop (*i.e.* $(\tilde{x}, \tilde{y}) = (0.5, 0.5)$) lateral diameter in the CA mode for different inter-droplet spacings. (b) The total dissolution time (T_i) of the droplets along the stream-wise direction. T_i is normalized using $T = \max(T_i)$. Note: Due to the limitation of the optical window, only the first seven droplets in one row can be captured in the case of $S = 2D_0$. (c) The relationship of T_i with S . T_i is normalised by the dissolution time (T) for the spacing of $S = 0.25D_0$ and S is normalised by D_0 .

immediately observed from both experiments and simulations that the center droplet (*i.e.* $(\tilde{x}, \tilde{y}) = (0.5, 0.5)$) with the largest spacing $S = 2D_0$ has a sharper dissolution slope than in the closely spaced array. Notably, the dissolution delayed along the flow direction has also been influenced. Fig. 5(b) summarizes the T_i of the droplets in the central column with the corresponding S . The following features are revealed from both experimental and numerical results: (i) the lifetime of the droplets is significantly decreased as the spacing is increased due to better accessibility of the flow; (ii) the lifetime of the last droplet is extended only in a closely packed array (*i.e.*, $S = 0.25D_0$ and $S = 0.5D_0$); (iii) the sequential dissolution along the flow direction is more pronounced in the closely packed array. All the evidence here shows that the stronger collective effects occur in a closely packed array as compared to a loosely packed array.

To give a quantitative estimate of the dissolution time, the total dissolution time of the central droplet T_i is plotted *versus* the spacing S in Fig. 5(c). The experimental data are in good agreement with the numerical simulations, showing that the dissolution time decays along with increasing spacing between the droplets. The dissolution rate of the droplet can increase up to 60% as S increases from $0.25D_0$ to $20D_0$. It is expected that with a large spacing between the droplets, the wake and the incoming flow for every drop is relatively fresh in comparison with closely packed droplets. This leads to a higher local concentration gradient which in turn enhances the dissolution rate and thus reduces the droplet lifetime.

3.4 Influence of external flow rate

Finally, the rate Q of the fresh water flowing through the microchamber is varied. For a different Reynolds number Re

$= Q/(wv)$, the time evolution of the lateral diameter for the central droplets ($(\tilde{x}, \tilde{y}) = (0.5, 0.5)$) is illustrated in Fig. 6(a), as a representative case. Overall, the total dissolution time decreases at higher Re . As mentioned earlier, the droplets along the stream-wise direction have shown delayed dissolution in the closely packed pattern with $S = 0.5D_0$ under $Re = 0.07$ and $Re = 0.15$. (Fig. 6b, black and blue curves). When the Re increases to 0.22, each drop starts to shrink simultaneously without dependence on droplet location (Fig. 6b), suggesting that the reduction of the local concentration gradient in the droplet array is more homogeneous due to a faster external flow. Such a feature is evidence that a faster external flow becomes dominant for droplet array dissolution, which has smeared out the local collective effect. Additionally, for a given array, the dissolution time T_i scales as $T_i \propto Re^{-3/4}$ (Fig. 6c). This scaling reflects a laminar flow of the Prandtl–Blasius–Pohlhausen type in the system.³⁴

3.5 Microlens arrays with a gradient structure

Before concluding the paper, we will demonstrate a potential application of the droplet array dissolution, namely, in the fabrication of microlens arrays with a curvature gradient. Microlens-gradient arrays have superior optical properties for real-time 3D imaging,³⁵ wide field optics,³⁶ and selective light harvesting. Owing to lenses with different curvatures integrated into one array, the focal plane of the microlens gradient array can be curved, largely overcoming the field curvature aberration from conventional microlens arrays with a flat focal plane.³⁷ Such a complicated lens array structure has been achieved by using sophisticated femtosecond laser direct writing technology.³⁸ Herein, we propose a novel, simple

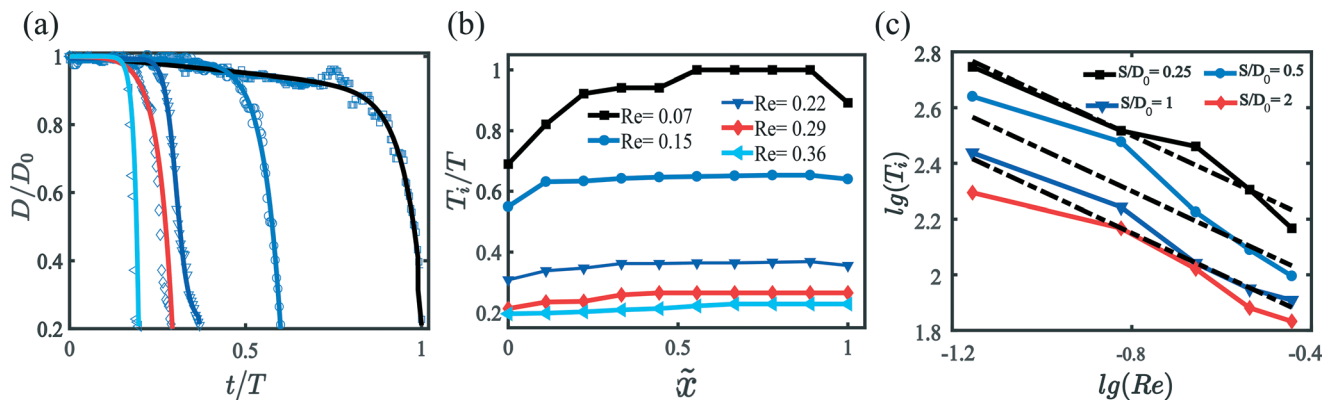


Fig. 6 (a) Experimental dissolution curves for the central droplet $(\tilde{x}, \tilde{y}) = (0.5, 0.5)$ in the CA mode under different flow rates, expressed in terms of Re for $S = 0.5D_0$. (b) The total dissolution time (T_i) of the droplets along the stream-wise direction under a corresponding Re value. T_i is normalized using $T = \max(T_i)$. (c) The experimental results of the total dissolution time T_i of the central droplet with $(\tilde{x}, \tilde{y}) = (0.5, 0.5)$ as a function of Re on a log–log plot for a different droplet spacing S as indicated. The dashed line shows the scaling law $T_i \propto Re^{-3/4}$.

and cost-effective method to generate microlens gradient arrays, simply based on droplet dissolution.

As discussed in the earlier sections, because of strong collective and flow effects, the droplets on the closely packed array at each location can experience different dissolution phases, which leads to various droplet curvatures on a single array. The corresponding morphology of the droplets has been well preserved by fast photopolymerization, resulting in microlenses on an array with gradient curvatures. Fig. 7(a) shows the optical images of formed microlens arrays. The different colours and numbers of the Newton rings on each droplet clearly represent

their different curvatures, which implies the multifocus available on a single microlens array. As a proof of concept, we tested that the obtained arrays with a microlens gradient display asymmetrical diffraction patterns under white light illumination (Fig. 7(b)). The levels of the diffraction order increased along with the height or size of the microlenses which increased from the left side to the right side of the substrates. This simple demonstration shows the great potential of selectively manipulating the pathway of light using microlens arrays with gradients, which will be significant to many optical applications.

4 Conclusions

In summary, we have quantitatively demonstrated how the dissolution of femtoliter surface droplet arrays depends on the droplet location, the spacing between them, and the imposed flow rate. The combined influence of collective effects and flow conditions on the lifetime of femtoliter droplet arrays has been quantitatively analysed *via* comparison of experimental and numerical results, which are quite consistent. Droplets surrounded with more neighboring drops take longer to dissolve, due to the collective effects as the droplets sense their neighbors through the surrounding flow field which is affected by the wake and the incoming flow. Such collective effects become more pronounced in a more closely packed array, in which the lifetime of droplets is further extended. The collective effects are also reflected in the dissolution rates of the droplets in a row along the flow direction or across the flow direction; in the latter case, the droplets at the edge dissolve faster. The overall dissolution is clearly accelerated by increasing the flow rate in all cases, implying that the reduction of the local concentration gradient is enhanced by applying an external flow. The immersed boundary method (IBM) code developed in this work will have a predictive power for the dissolution of droplets with various initial

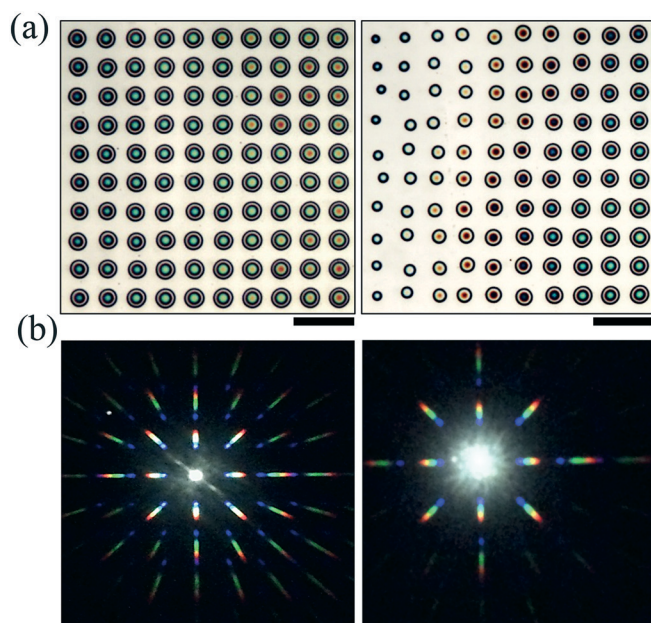


Fig. 7 Gradient microstructure based on droplet array dissolution: (a) optical images of dissolved microlens arrays and (b) the corresponding diffraction patterns. The scale bars are 30 μm .

sizes and spatial arrangements, far beyond what is already covered in our experiments.

Apart from our demonstrated fabrication of unconventional microlens arrays with optical advantages, the quantitative and in-depth understanding of the droplet dissolution in this work is highly valuable for many other droplet-based processes. In particular, the external flow and droplet spatial arrangement can be potentially manipulated to achieve uniform or gradually varying dissolution rates of individual droplets in the array. We envisage that gradually varied dissolution rates can be applied to effectively screen conditions for the crystallisation of pharmaceutical products, micro-diagnostics, self-assembly of nanoparticles or micro-compartmentalized chemical reactions.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

We thank Shantanu Maheshwari for support and discussions on the numerical simulations. L. B. acknowledges the support from the RMIT Vice Chancellor Postdoctoral Fellowship. X. H. Z. acknowledges support from the Australian Research Council (ARC, FT120100473). X. H. Z. and L. B. acknowledge support from ARC LP140100594. We would also like to thank Martin Klein Schaarsberg for assistance with data analysis, Dr. Qiming Zhang for help on the testing of optical properties and the RMIT MicroNano Research Facility (MNRF) for technical support. This work was supported by the Netherlands Center for Multiscale Catalytic Energy Conversion (MCEC), an NWO Gravitation programme funded by the Ministry of Education, Culture and Science of the government of the Netherlands. We acknowledge NWO for granting us computational time on the Cartesius cluster from the Dutch Supercomputing Consortium SURFsara.

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